

## Review

# Biogas/Biomethane Quality and Requirements for Combined Heat and Power (CHP) Units/Gas Grids with a Special Focus on Siloxanes-a Short Review

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**Abstract:** The presence of siloxanes in biogas and biomethane is a major barrier to using them as renewable energy sources in Combined Heat and Power (CHP) units and national grid systems. Siloxanes in the form of methyl siloxanes (including L2, L3, L4, D3, D4, D5, D6), Trimethylsilanol (TMSOH), as well as other contaminants such as H<sub>2</sub>S, NH<sub>3</sub>, relative humidity (rH), halogenated compounds (including organic chlorine and fluorine), and volatile organic compounds (VOCs) present in biogas upgraded to biomethane quality are detrimental to engines, turbines, and gas grids; therefore, it is necessary to remove them before their high-value utilization. Under oxidation, siloxanes are converted into microcrystalline silicon dioxide (SiO<sub>2</sub>) deposits that can shorten the lifetime of the engine and affect the gas grids. The review presents the actual requirements for biogas and biomethane quality in the context of their utilization in CHP units and national gas grids. Moreover, the methods of siloxane removal based on adsorption, absorption, cryogenic condensation, membranes, and biofiltration are described.

**Keywords:** biogas, biomethane, siloxanes, CHP units, biogas purification

## 1. Introduction

Nowadays the biomethane is gaining popularity.<sup>1</sup> The purification of biogas from siloxanes and its upgrading to biomethane becomes a real alternative for commercial biogas utilization. Moreover, several standards are describing the purity of biogas and biomethane originated from biogas upgrading.<sup>2</sup> On the other hand, the combustion of biogas/biomethane under the oxidation process is converted to carbon dioxide and water and in a natural way, the emission impact<sup>3</sup> is reduced. As the European Biogas Association (EBA) reported, biogas and biomethane have significant and growing contributions to achieve the European Union (EU) climate-neutrality by 2050 as well as, biogas industries have a significant impact on worldwide greenhouse gas reduction-potential to reduce Green House Gas (GHG) emissions is estimated by 10-13%.<sup>4</sup>

The review provides the parameters and requirements of biogas and biomethane in context to its utilization and direct injection to national gas grids systems. Moreover, the paper describes critical parameters of biogas quality in terms of manufacturer limitations and guarantees. The presented work describes the most popular biogas purification technologies based on physical, chemical, and biological processes with a special focus on siloxanes.

## 1.1 Parameters of biogas/biomethane as biofuel used in CHP units gas grids

The use of biogas/biomethane as a biofuel in CHP units producing electricity and heat requires a prior detailed analysis of the biogas with respect to the qualitative energy parameters of the raw material and the content of its pollutants. Biogas/biomethane used as a fuel in power generation units or injected into national gas grids needs to fulfill the strictly defined criteria of its utilization, in accordance with the manufacturer's guidelines or national grids limitations.<sup>5</sup> The unit manufacturer's guidelines describe in detail the biogas parameters that qualify the gas as a fuel of a given category: *low*, *medium*, and *high*.<sup>6</sup> The classification of biogas into one of the above categories has a direct impact on the engine's operating time between mandatory maintenance intervals, while at the same time showing an indirect-economic-character related to the cost of its servicing, replacement of its worn parts or lubricating oil. The frequency of mandatory technical maintenance of the unit depends mainly on the manufacturer of the power generation units, but most manufacturers declare that the mandatory maintenance interval should be carried out once every 4 months of uninterrupted operation of the unit. In the case of power generation units or CHP units, the period of the obligatory maintenance interval depends only on the quality of the raw material fed to the engine, respectively according to the following table: *Low*: mandatory service every 1000 hours of operation of the unit, *Medium*: mandatory service every 3000 hours of operation of the unit, *High*: mandatory service every 5000 of operation of the unit.<sup>6</sup>

Determination of the energy value of the raw material and the level of classification of the biogas is important investment information based on which the model, the type, and the power of the unit are evaluated, and a maintenance schedule is established together with a cost estimate. Tables 1, 2, and 3 below present detailed guidelines for the quality of the propellant fed to the unit for the power generating units of leading European manufacturers.<sup>6</sup> The following parameters apply also to those systems that are equipped with CHP with a small and micro scale, but the range of the pollution limits is significantly weaker.

**Table 1.** Boundary parameters for biogas used in the CHP units<sup>6</sup>

Parameter	Unit	Limit
	Calorific value kWh/m <sup>3</sup>	> 5
Methane content	Calorific value H [MJ/m <sup>3</sup> ] (0 °C, 101,335 kPa)	Wu > 18
	Vol %	40-70, < 90
H <sub>2</sub> S	ppm	< 200
Total Sulphur	mg/m <sup>3</sup> N	< 200
Halogens (Cl, Br, F, I)	mg/m <sup>3</sup> N CH <sub>4</sub>	< 80
Dust	mg/m <sup>3</sup> N CH <sub>4</sub>	< 10
	<i>grain</i> < 5 μm	
Oil mist (OM)	mg/m <sup>3</sup> N CH <sub>4</sub>	< 400
VOCs	mg/m <sup>3</sup> N CH <sub>4</sub>	< 25
Silicon content (Si)	mg/m <sup>3</sup> N CH <sub>4</sub>	< 2
Relative humidity	rH % / °C	< 80
Ammonia	mg/m <sup>3</sup> N CH <sub>4</sub>	< 30
Gas temperature	°C	10 < T < 30
Oxygen content	%	< 2

The units in which the pollutants are described, i.e. mg/m<sup>3</sup> N CH<sub>4</sub> as well as mg/10 kWh, are used alternately by the manufacturers and are equivalents.

**Table 2.** Limiting parameters for biogas used in the Power Generation units<sup>6</sup>

Parameter	Unit	Limit
Methane content	Caloryfic value kWh/m <sup>3</sup>	> 5
	Vol %	> 50
H <sub>2</sub> S	ppm/10 kWh	< 1500
Sulphur which is not a derivative of H <sub>2</sub> S	mg/10 kWh	-
Halogens (Cl, Br, F, I)	mg/10 kWh	< 100
Dust	mg/10 kWh	< 10
	<i>grain 3-10 µm</i>	
OM	mg/10 kWh	< 400
Silicon compounds (Si)	mg/10 kWh	< 20
Relative humidity	rH % / °C	< 80
Ammonia	mg/10 kWh	< 30

**Table 3.** Pollutant limit parameters for quality classification of biogas used in the CHP units<sup>6</sup>

Gas quality/Parameters	Low	Medium	High
Sulphur (total S) per 10 kWh	below 2200 mg	below 440 mg	below 15 mg
Hydrogen sulphide (total H <sub>2</sub> S) with reference to 10 kWh	above 1500 ppm (corresponds to 0.15 vol. %)	below 300 ppm (corresponds to 0.03 vol. %)	10 ppm (corresponds to 0.001 vol. %)
Chlorine (total Cl) per 10 kWh	below 100 mg	below 20 mg	below 2 mg
Fluorine (total F) per 10 kWh	below 50 mg	below 10 mg	below 1 mg
Chlorine and fluorine (total Cl and F) per 10 kWh	below 100 mg	below 20 mg	below 2 mg
Ammonia (total NH <sub>3</sub> ) per 10 kWh	below 150 mg	below 30 mg	below 2 mg
Humidity	below 80%	below 50%	below 50%
Silicon compounds (VMSs) per 10 kWh	below 20 mg	below 1 mg	0 mg
Dust content. Total per 10 kWh	below 10 mg	below 2 mg	below 0.5 mg
Dust granularity	above 3 µm	above 2 µm	above 2 µm
Higher hydrocarbons and tars above C5/below C10 per 10 kWh	below 3000 mg	below 600 mg	below 100 mg
higher/equal C10 per 10 kWh	below 250 mg	below 50 mg	below 10 mg
higher/equal C12 per 10 kWh	below 0.5 mg	0 mg	0 mg

Apart from its energy properties, biogas has a very complex organic matrix. This matrix contains over 400 different compounds of organic origin-from simple hydrocarbons to complex terpene derivatives.<sup>7</sup> On the other hand, the presence of chemical compounds such as hydrogen sulphide, ammonia, halogens, Oil Mist (OM)-hydrocarbons with more than 10 carbon atoms in the molecule, silanes, methyl siloxanes, or trimethylsilanol (TMSOH)-has a significant impact on the efficiency of biogas energy production. Most organic pollutants which are present in biogas are formed by the decomposition of substances contained in organic matter and are of different polarity, water-solubility, volatility, or vapor pressure, which creates particular difficulties in their control, determination, or removal. Besides, when considering the use of biogas as a fuel in biogas engines, the influence of the matrix and the effect of gas impurities on the efficiency of the extracted energy must be taken into account, both technologically and economically.<sup>8</sup> The content

of more or less problematic compounds in biogas leaves its mark in the form of reduced efficiency of the unit, shorter intervals between compulsory maintenance, or plant downtime due to the replacement of internal parts of the plant or the unit. The requirements for biomethane are listed in Table 4.

**Table 4.** Biomethane injected to gas grid requirements<sup>9,10</sup>

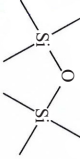
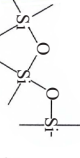
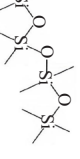
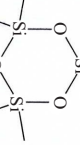
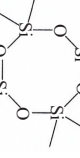

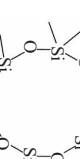
Parameter	Biomethane	EU Standards
Higher heating values (MJ/Nm <sup>3</sup> )	37.2 ± 0.6	
Wobbe index (MJ/Nm <sup>3</sup> )	50.2 ± 1.9	
Methane number (MN)	95 ± 4.2	> 65.0
Relative density	0.54 ± 0.02	
CH <sub>4</sub> (v/v%)	97.4 ± 2.4	> 45.0
CO <sub>2</sub> (v/v%)	1.1 ± 0.3	< 45.0
O <sub>2</sub> (v/v%)	0.1 ± 0.05	< 0.1
N <sub>2</sub> (v/v%)	0.05 ± 0.01	
H <sub>2</sub> (v/v%)	0.05 ± 0.02	< 2.0
H <sub>2</sub> S (ppm)	88.1 ± 2.0	
Mercaptans (as S) (mg/Nm <sup>3</sup> )	0.2 ± 0.1	
Total S (mg/Nm <sup>3</sup> )	88.1 ± 2.2	
CO (mg/Nm <sup>3</sup> )	0.02 ± 0.01	
Siloxanes (mg/Nm <sup>3</sup> ) as VMSs	0.05 ± 0.02	< 0.79
NH <sub>4</sub> (mg/Nm <sup>3</sup> )	1.1 ± 0.1	
VOCs (mg/Nm <sup>3</sup> )	63 ± 5.9	
Fluorine (mg/Nm <sup>3</sup> )	9.2 ± 1.0	
Chlorine (mg/Nm <sup>3</sup> )	80.0 ± 5.2	
Dew point (%) at 27 °C	22.2 ± 0.1	> 90.0

## 2. Siloxanes in biogas/biomethane

The influence of silicon compounds and other impurities present in biogas on energy and heat production in the process of cogeneration.<sup>11</sup> The presence of volatile silicon compounds in biogas/biomethane poses very serious problems for biogas power generation units and national gas grids for operators. During the process of biogas/biomethane utilization, a number of chemical reactions involving volatile silicon compounds take place in the units. The main reaction of siloxanes in the biogas is oxidation, where the final product in the shape of the microcrystalline deposit of SiO<sub>2</sub> is formed.<sup>7</sup> The microcrystalline deposit from the combustion chamber is characterized by the presence of elements such as calcium, bismuth, zinc, and Sulphur, in addition to a predominance of SiO<sub>2</sub>. Most of the analyzed motor deposits are white or slightly grey in color. The morphological structure of the surface varies depending on where it is formed. We distinguish between deposits with different physical structures, ranging from perfectly smooth through clusters to completely heterogeneous. Microcrystalline SiO<sub>2</sub> in its various forms perfectly covers the internal parts of the engine, sometimes with a layer of several millimetres, which is difficult to be removed. The tendency to form a thin microcrystalline film depends mainly on the internal combustion chamber temperature, the pressure inside the chamber, the catalyst used, or the type of surface exposed to adhesion. In addition, the layer of microcrystalline SiO<sub>2</sub>

deposited on the internal parts of the unit acts as an insulator, preventing proper cooling of the unit, which consequently leads to overheating of the running engine components. The most exposed to microcrystalline sludge are the following: combustion chambers, valves, valve seats, cylinder crowns, cylinder walls, piston crowns, and pans-these are also the hottest parts of a running engine. In the case of biomethane, siloxanes cause damage to gas grids.<sup>7,10</sup>

**Table 5.** Physical and chemical properties of siloxanes<sup>12</sup>

Name	Hexamethyl-Disiloxane (L2)	Octamethyl-Trisiloxane (L3)	Decamethyl-tetrasiloxane (L4)	Hexamethylcyclo-trisiloxan (D3)	Octamethylcyclo-tetrasiloxan (D4)	Decamethylcyclo-pentasiloxane (D5)	Dodecamethylcyclo-hexasiloxane (D6)
Structure							
Molecular formula	C <sub>6</sub> H <sub>18</sub> O <sub>Si</sub> <sub>2</sub>	C <sub>8</sub> H <sub>24</sub> O <sub>3</sub> Si <sub>3</sub>	C <sub>10</sub> H <sub>30</sub> O <sub>4</sub> Si <sub>4</sub>	C <sub>6</sub> H <sub>18</sub> O <sub>3</sub> Si <sub>3</sub>	C <sub>8</sub> H <sub>24</sub> O <sub>4</sub> Si <sub>4</sub>	C <sub>10</sub> H <sub>30</sub> O <sub>5</sub> Si <sub>5</sub>	C <sub>12</sub> H <sub>36</sub> O <sub>6</sub> Si <sub>6</sub>
Physical properties	Liquid, colorless, odorless	Liquid, colorless, odorless	Solid	Solid, white, hydrocarbon odor	Liquid, colorless, oily, odorless	Liquid, oily	Liquid, colorless, faint odor
Molecular weight (Da)	162.38	236.54	310.7	222.47	296.61	370.80	444.93
Boiling point, °C	101	153	193.95	135	175.5	210	245
Melting point, °C	-59	-82	No data	64	17.5	7.5	-3
Water solubility mg/L at 23 °C	0.93	0.034	0.006 (at 25 °C)	1.56	0.056	0.017	0.005
Vapor pressure, mm Hg at 25 °C	42.2	13.90	0.43	3.53	1.05	0.20	0.049
Henry's constant (atm m <sup>3</sup> /mol)	2.4 ± 0.2, at 27 °C	121 ± 12, at 27 °C	No data	No data	24 ± 3, at 28 °C	12 ± 2, at 26 °C	5.9 ± 2.9, at 26 °C

The formation process of microcrystalline precipitate during the oxidation of VMSs inside the generator is described in two steps. In the first stage, in a combustion chamber, volatile methyl siloxanes are oxidized under high temperature and pressure to an amorphous, liquid form of microcrystalline glass. The second stage is the crystallization process, which takes place after the engine has cooled down; during this stage, with the slow process of cooling, the amorphous form crystallizes, covering the internal parts of the unit with a thin deposit layer. The deposit does not spread regularly inside the unit; its occurrence depends mainly on the cooling rate of the internal parts of the unit. Most of the deposit is accumulated in the combustion chamber on pistons and cylinders, while its uneven distribution disturbs the combustion geometry of the chamber resulting in the disorderly knocking forces and, as a consequence, inhomogeneous combustion of biogas and, hence, generates higher emission of pollutants into the atmosphere.<sup>7</sup>

At the same time, other pollutants present in biogas, such as oil mist, halogens, hydrogen sulphide, dissolve in the rH present in biogas, forming organic and inorganic acids ( $\text{H}_2\text{S}_{\text{aq}}$ ,  $\text{HCl}_{\text{aq}}$ ,  $\text{HF}_{\text{aq}}$ ), which as being present in the engine oil, drastically reduce its lubricating properties. In Table 5 physical and chemical properties of siloxanes presented in biogas/biomethane are presented.<sup>12</sup>

In the biomethane context, the initially pre-treated biogas (with low humidity) requires strong purification to be forwarded to the membrane upgradation system. Moreover, it must be taken into account that there are several local and EU standards to describe the purity of biomethane originating from biogas upgrading, which refers to the limitation of biomethane impurities in detail.<sup>10</sup> As the EBA reports, biogas and biomass industries have a significant and growing role in achieving climate neutrality by 2050. These industries significantly impact worldwide greenhouse gas reduction: Their potential to reduce greenhouse gas emissions is estimated to be around 10-13%. Moreover, upgrading biogas to biomethane serves as an example to understand the concept of “short carbon cycle”.<sup>10</sup>

### 3. Removal of volatile methyl siloxanes from biogas/biomethane

Describing the methods for the removal of Volatile Methyl Siloxanes (VMSs) from biogas/biomethane, several commonly used techniques were taken into account. They include the occurring biological, physical, or chemical phenomena, as well as the physical and chemical properties of VMSs.<sup>13</sup>

The correlations between the physicochemical properties of VMSs and the physical and biological phenomena have been presented below. The commonly used methods for removing VMSs from biogas are based on them.

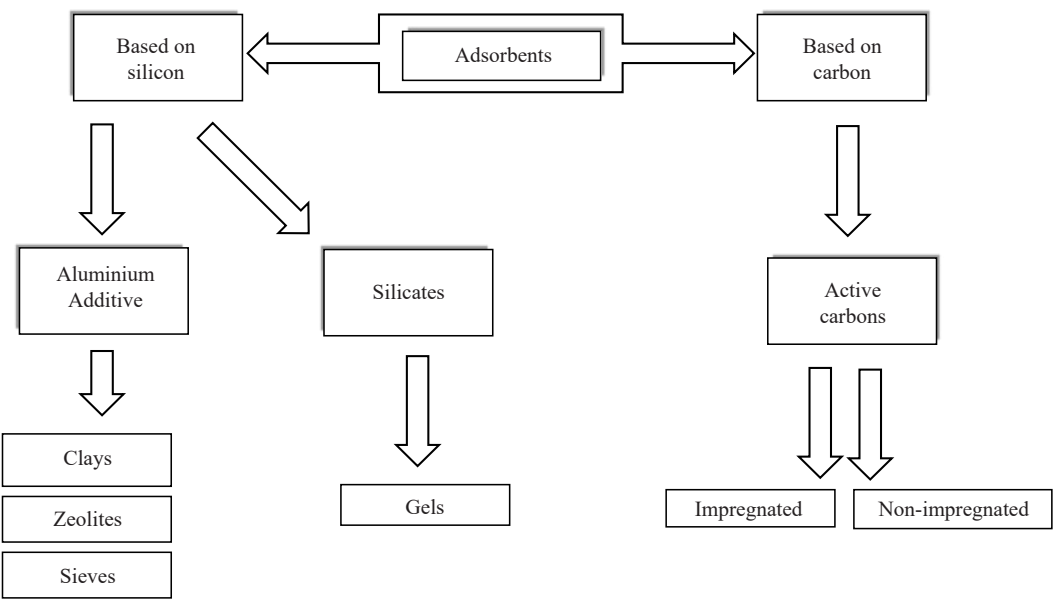
Since 2020, it could have been found in the literature that there are three commercial concepts describing the proposals of silica-contaminants solutions based on absorption and adsorption technologies.<sup>14</sup> However, the most popular and common applied technologies for silica-contaminants removal being in common use are based on adsorption on activated carbon.

#### 3.1 Removal of VMSs based on the adsorption

One of the most popular methods for removing VMSs is based on the phenomenon of physical adsorption of methylsiloxane molecules on the inner and outer surfaces of adsorbent materials, which largely depends on the porosity of the adsorbent. Figure 1 presents a classification of adsorbents commonly used in the process of methylsiloxane removal from biogas due to their chemical structure. Adsorption on active or activated carbon is one of the most commonly used biogas purification technology. However, the adsorption process strongly depends on the properties of used carbons. In general, the adsorption on porous material is strongly associated with its surface area and type-size of pore.<sup>15</sup> The important issue has been noticed in the works of Ajhar et al.<sup>13</sup> They reported that the absorption process of siloxanes on active/activated carbon depends on siloxanes concentration, type of active carbon impregnation, the water content of biogas, and temperature.<sup>13</sup>

Further adsorbents commonly used in biogas purification technology include carbon-based sorbents such as activated carbon, graphite, or coke nutshells. Considering the most technologically common activated carbon, it is characterised by a well-developed specific surface area of up to 1600 m<sup>2</sup>/g and a highly developed porous structure. It is a very universal sorbent, used extensively in biogas treatment systems with VMSs. However, it does not entirely account for its advantages and more specifically its superiority over other silicon-based adsorbents. Its main disadvantage is the lack of selectivity towards the adsorption of VMSs. As studies have revealed, the efficiency of adsorption of VMSs by

activated carbons ranges from 5000 to 15000 mg<sub>siloxane</sub>/kg of carbon, while maintaining the parameters of appropriate pressure and temperature, resulting in a real efficiency of the adsorption process at the level of 0.5-1.5% by weight of the filter used. Another technological barrier to using coal in the gas purification process is the requirement to remove excess moisture from the biogas stream entering the coal filter. Excessive moisture considerably reduces the efficiency of the filter by blocking the sorption surface with water molecules, which in turn considerably reduces the efficiency of the adsorption process.<sup>16</sup> On the other hand, activated carbon that is additionally impregnated-by covering its surface with a suitable chemical compound (e.g. KI or NaOH)-acquires additional properties that allow hydrogen sulphide in the process of the removal through the alkalimetric acid/base reaction.<sup>17</sup> As it has been proved, in the case of VMSs removal (except trimethylsilanol-TMSOH) on an impregnated filter, appropriately coated activated carbon has a lower adsorption efficiency and significantly decreases the filter efficiency. The most significant advantages of using carbon filters in commercial gas purification technologies are its low price, availability, and the low-cost process of its thermal regeneration.<sup>17</sup> The following Table 6 presents the above described commercially used VMSs adsorbents and compares them with each other in terms of structure, polarity, porosity, specific surface area, and pore size.



**Figure 1.** Division of VMS adsorbents according to their chemical structure

**Table 6.** Selected physical properties of VMSs adsorbents<sup>18</sup>

Adsorbent	Structure physical	Polarity	Porosity (%)	Specific surface area (m <sup>2</sup> /g)	Pore size (nm)
Silica gels	amorphous	polar	70	750	2.2
Molecular sieves	crystal	polar	40-55	600-700	3.0-9.0
Active carbons	amorphous	non-polar	55-75	600-1600	1.5-2.0



### 3.2 Removal of VMSs based on chemical and physical absorption

The removal of VMSs based on the phenomenon of chemical absorption in a liquid medium has been attempted several times by different researchers.<sup>19</sup> Chemical absorption of volatile methyl siloxanes from biogas based on the use of concentrated acids and alkalis has not yet proved to be an effective method for biogas cleaning. On the other hand, taking into account the chemical stability of the siloxane chain, the removal process of VMSs based on its direct dissociation (also in strong acids and bases) may not be efficient, given the high ionization energy of the Si-O.

### 3.3 Removal of VMSs based on biological processes

The removal of VMSs from biogas based on biological processes<sup>20</sup> is an alternative to the methods commercially used in biogas treatment technology, however, the biodegradation method has several significant limitations that require further scientific and technological recognition. Although VMSs show relative resistance to chemical and biological degradation reactions, techniques are known for their removal based on biological processes. Laboratory biofilters are based on microorganisms living in the aquatic environment tj. *Pseudomonas* (*P. aeruginosa*, *P. fluorescens*, *P. Putida*) *Agrobacterium* (*A. radiobacter*), *Arthobacter* or *Fusarium oxysporium*, whose main problem of their adaptation under technological conditions is the high flow rate and thus the very short contact time of the bacterial flora with the VMSs particles, allowing the initiation of degradation bioreactions. Laboratory biofilter-based methods indicate to remove a maximum of 50% of the total VMS load from the inlet biogas stream, assuming a very low biogas flow rate of typically more than the level of 0.5 l/h. Most operations on the biological degradation of VMSs are based on the degradation of cyclic D3 or D4. Micro-organisms based biological degradation of decamethylcyclopentasiloxane where the final reaction product is silicic acid ( $\text{H}_4\text{SiO}_4$ ) and formaldehyde. The operation of the biofilter, however, has its significant limitations, representing a low level of performance for VMSs characterised by low solubility in water, which in fact represents a major barrier to the commercialisation of a technological biofilter solution for the removal of VMSs. As it has been confirmed by scientific studies, the removal efficiency of VMSs from biogas in biological processes can be significantly improved by enriching the biofilter with non-ionic substances, e.g. oleic alcohol. As it has been scientifically proven, in most cases the implementation of biofilters for VMS removal from biogas is still at the design stage, among which the biggest obstacle is to obtain high VMS removal efficiencies with full biogas process flows of up to 1000 m<sup>3</sup>/h.<sup>20</sup>

### 3.4 Removal of VMSs based on cryogenic condensation

Cryogenic condensation is one of the methods where the deep chilling of biogas/biomethane was reported. Schweigkofler and Niessler<sup>19</sup> investigated the siloxanes removal efficiency at 5 °C and over 88% of the initial siloxane concentrations remained. Hagmann et al., reported a cleanup efficiency for a range of volatile siloxanes of 25.9% when cooled down to -25 °C. Rossol et al., operated deep chillers to remove siloxanes from sewage-sludge biogas at a working temperature of -30 °C and reported elimination rates of 80%-90%.<sup>22</sup> As recent literature indicates, the Cryogenic Temperature Condensation System (CTCS) based on two chilling columns was tested and the siloxanes from the biogas stream were removed entirely.<sup>10</sup> The temperature of the process on -50 °C and the biogas flow is up to 100 dm<sup>3</sup>/h. The CTCS works in temperatures ranging from -50.0 to +40.0 °C and formed condensate discharges automatically from internal parts of the column.<sup>10</sup>

### 3.5 Other methods of VMSs removal from biogas

The market demand for a simple, sustainable, and environmentally friendly method for the commercial efficient removal of volatile silicon compounds, which at the same time includes an economic optimum, is the basis for advanced research on biogas and the VMS contained therein. Research reports indicate several new ideas that, for the time being, still do not go beyond the laboratory environment.

One interesting alternative to physical processes involves processes using combustion reaction catalysts VMSs. A catalyst in the form of  $\text{V}_2\text{O}_5$  adsorbed on  $\text{TiO}_2$  together with biogas heated to a temperature in the range of 250-400 °C allows for the removal of the silicon charge along with other organic impurities prior to direct feeding of the biogas to



the unit. The only disadvantage of the combination used is the rapid wear of the catalyst, due to its surface coating with microcrystalline SiO<sub>2</sub>. Another way of removing VMSs in the form of D3 was to use catalysts in the form of oxides, i.e. CaO, MgO, Al<sub>2</sub>O<sub>3</sub>, however, the operation of the catalysts at 200-400 °C did not show significant removal efficiencies of VMSs.<sup>23</sup>

Research carried out on membrane technology<sup>24</sup> for the removal of VMSs is still in the laboratory testing phase, but it offers a real opportunity for implementation. The promising approach was conducted on the poly-dimethyl-siloxane membrane, which can be adopted for siloxanes (the membrane was tested on octamethyl tetrasiloxane) and VOC removal from biogas, but further tests should be led.<sup>25</sup>

Researches over methods of removing VMSs from biogas reveals three more completely new ways of cleaning biogas. The first of these is ultraviolet photodecomposition,<sup>26</sup> in which silicon compounds are already removed from the production waste. The second method is based on peroxidation,<sup>27</sup> where the removal efficiency of D4 and D5 is up to 50% and the third anode is solid oxide fuel cell anode degradation,<sup>28</sup> however, the efficiency of Si-contaminants removal for proposed solutions was up to 25% or was more efficient for chosen types of siloxanes.

## 4. Conclusion

The conclusion was drawn from the work that biogas and biomethane are the energetic media that need to be cleaned from siloxanes before their utilization. Presently, the most common and applied in industry method of siloxanes removal is cleaning using active carbon filters. Moreover, further research should be focused on methods based on biological processes, membrane separation, catalytic reactions, peroxidation, or anode degradation with taking into account the selectivity of siloxanes, thus it depends on biogas origin. An improvement for purification technology based on effective siloxanes removal systems is central to protect CHP units and gas grids as well as upgrade the biogas to biomethane quality.

## Conflict of interest

The author declares no conflict of interest.

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